

The Influence of Air Dilution with Nitrogen on Hydrogen Jet Ignition

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1 Introduction

Pressurized hydrogen jet release into atmospheric air is associated with many engineering applications, such as high-pressure storage vessels [1] and nuclear power plant safety during a severe cooling system malfunction [2]. Discharge of pressurized hydrogen from a vessel into the ambient leads to formation of a strong shock wave, which is followed by the hydrogen jet. At the jet's head, a thin mixing diffusion layer δ between the hot air and the cold expanded hydrogen is formed, which is represented with a simplified sketch in Fig. 1. It is known that self-ignition typically occurs at the diffusion layer [3]. Nevertheless, the self-ignition process is complex and depends on the interplay between the heat release due to chemical reactions, which leads to a temperature rise, and the jet expansion process, which leads to a temperature drop [4]. Moreover, mass diffusion of the much lighter hydrogen into the hot air as well as conduction heat transfer also govern the self-ignition process.

Many efforts were devoted in recent years to explore the problem of self-ignition experimentally. Experiments involved either completely unconfined or confined conditions, where the pressurized jet is released from a tube [1, 5, 6]. It is now well-established that the self-ignition process is influenced by various parameters and, most importantly, by the downstream geometry. For example, the occurrence of ignition is affected by the tube length, hole release diameter, cross-section shape, and the opening process of the pressure vessel [1, 7, 8]. In addition, this unique phenomenon has been studied theoretically

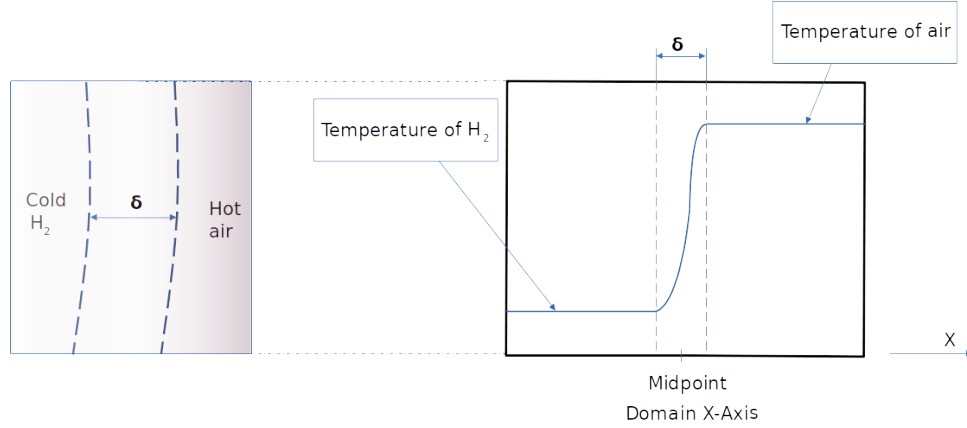


Figure 1: Schematic representation of the diffusion layer at the head of the hydrogen jet.

by various researchers to gain better understanding of the underlying physical phenomena that affect the ignition limits [1,4].

The scenario of pressurized hydrogen release into air can become even more complicated when the pressurized hydrogen is mixed with other gases and then released into the air. These more involved scenarios include pressurized release of hydrogen-methane [9] or hydrogen-nitrogen mixtures [1]. For both cases, the hydrogen dilution highly affects the ignition delay time. Nevertheless, the effect of inert gas dilution on the air side has never been explored. Thus, in the present work, we address this problem, and explore the effect of nitrogen dilution on the air side. In particular, we carry out and analyze in detail 1-D transient numerical simulations of the ignition process within the diffusion layer at the jet's head.

2 Numerical Solver and Governing Equations

Numerical simulations are conducted via the open source code - Ember. This code is designated for simulating 1-D unsteady reactive flows and provides superior performance for simulations with large multi-step chemical kinetic models [10]. As the diffusion layer is stagnant, in the jet's head frame of reference, see also [4], only the energy and species equations are solved. Thus, the momentum and mass conservation equations are not considered in the current study. The conservation of species is shown in Eq. 1:

$$\rho \frac{\partial Y_k}{\partial t} = -\frac{\partial j_k}{\partial x} + \omega_k W_k, \quad (1)$$

where Y_k is the mass fraction of species k , ρ is density, ω_k is the molar production rate of species k , W_k is the molar weight of species k , t is the time, x is the spatial coordinate, and j_k is the diffusive mass flux, which is presented in Eq. 2:

$$j_k = -\rho D_{km} \frac{\partial Y_k}{\partial x} - \frac{D_k^T}{T} \frac{\partial T}{\partial x} + Y_k j', \quad (2)$$

where D_{km} is the mixture-averaged diffusion coefficient, which provides a relation between the mass flux and the mass-fraction gradient, D_k^T is the thermal diffusion coefficient, T is the temperature, and j' is the correction term.

The conservation of energy, under the assumption of negligible viscous effects, is shown in Eq. 3:

$$\rho \frac{\partial T}{\partial t} + \frac{1}{c_p} \sum_{k=1}^K \hat{h}_k \dot{\omega}_k + \frac{1}{c_p} \sum_{k=1}^K j_k c_{p,k} \frac{\partial T}{\partial x} = \frac{1}{c_p} \frac{\partial}{\partial x} \left[\lambda \frac{\partial T}{\partial x} \right], \quad (3)$$

where λ is the mixture thermal conductivity, c_p and $c_{p,k}$ are the mixture and species specific heat capacities at constant pressure, respectively, and \hat{h}_k is the species molar enthalpy.

3 Problem setup and initial conditions

In the current work, we investigate numerical solutions for 1-D reactive and stagnant diffusion layers under conditions relevant for a pressurized hydrogen jet release scenario. Thus, the initial conditions mimic the conditions for diffusion ignition at the hydrogen jet's head, where one side contains pressurized hydrogen and the other side contains air diluted with nitrogen. The initial conditions are determined according to a 1-D shock-tube solution via the software package Cantera [11]. Note that we do not take into account the jet expansion during the release process itself. This approach provides insights on the fundamental problem dynamics at the early stages before significant jet expansion occurs, see also [12]. For all the cases, a pressure ratio of 400 was assumed between the pressurized hydrogen, in the driver section, and the ambient, in the driven section, with an initial temperature of 293 K for both gases. The domain size is 2 mm and the interface between the two gases is located exactly at the domain's center. Also, we used a uniform grid with 1200 cells and a time step of 1.0×10^{-10} s, which were found to be sufficiently small for capturing the changes in the reaction and diffusion terms. All the simulations were carried out at least until the ignition was achieved. Moreover, we found that by using a mixture averaged diffusion coefficient, we can achieve indistinguishable results in comparison with using the more computationally expensive multi-component diffusion coefficient. For all the simulations, we used the chemical mechanism of Burke et al. [13], which consists of initiation, chain branching and termination reactions.

The initial temperatures and the pressures at the diffusion layer, which were obtained via the shock-tube solution, are shown in Table 1. We investigated three different cases, where, in each case, the ambient air is diluted by a certain amount of nitrogen. The first case involves pure air, whereas the second and the third cases consist of mixtures with mole percentages of 88% N_2 with 12% O_2 and 94% N_2 with 6% O_2 , respectively. Pure hydrogen was used as fuel in the three different cases. One can see in Table 1 that the N_2 dilution on the air side has a negligible effect on the initial conditions. For instance, for 21% of O_2 , the pressure at the diffusion layer is equal 43.71 atm, and for the most diluted case with 6% of O_2 , a value of 43.43 atm is obtained. Hence, the differences between the initial temperatures are also very small. This is not surprising as N_2 and O_2 have very similar molar weights. Next, we present and analyze the resulting temperature and species-mass-fraction evolution for the different cases.

Table 1: Initial temperature and pressure profiles at the diffusion layer for diluted air side obtained from the shock-tube solution for a pressure ratio of 400.

Ambient composition	H ₂ temperature, K	Air temperature, K	Initial pressure, atm
21% O₂, 79% N₂	150.65	2100	43.71
12% O₂, 88% N₂	150.34	2098	43.43
6% O₂, 94% N₂	150.14	2097	43.24

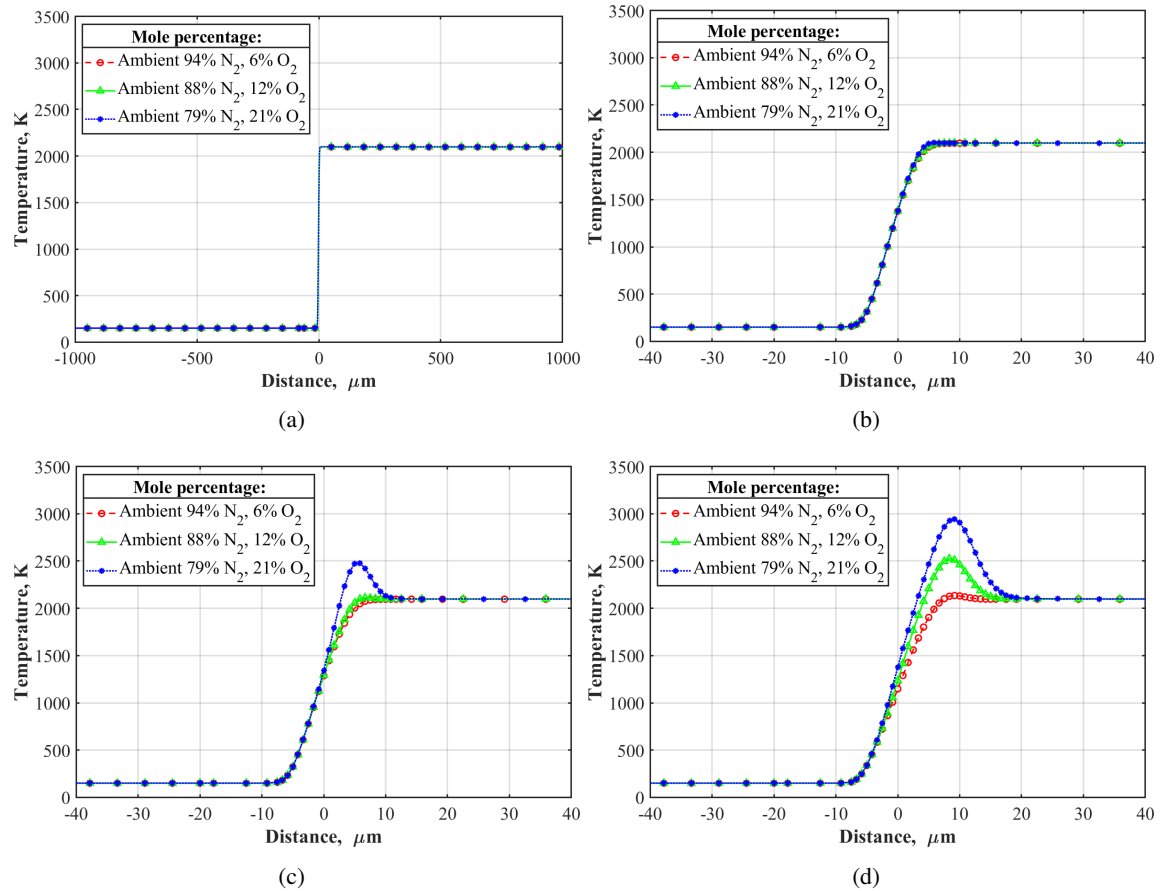


Figure 2: Temperature profiles in the diffusion layer region at (a) $t=0 \mu\text{s}$, (b) $t=0.06 \mu\text{s}$, (c) $t=0.10 \mu\text{s}$, and (d) $t=0.20 \mu\text{s}$.

4 Results

Figure 2 shows the temperature profiles for all the cases at different time instants. At time $t=0 \mu\text{s}$, the initial profiles are almost identical, see Fig. 2(a). Note that the nitrogen dilution influence on the initial conditions is negligible due to the almost identical speed of sound for all the cases, which leads to an almost identical shock-wave strength. After $0.06 \mu\text{s}$, hydrogen diffuses rapidly within the diffusion layer due to its low molecular weight. The hot air and cold hydrogen mix and heat transfer occurs through conduction. As a result, the hydrogen heats up gradually and starts reacting with the oxygen in the air. As the hydrogen and oxygen react with each other, more heat is released, which further increases the temperature of the mixture and leads to a self-ignition process. The temperature increase or the so-called “hump” shown in Figure 2(b), for the pure-air case, demonstrates the self-ignition process. At $0.10 \mu\text{s}$, see Figure 2(c), the diluted case with 12% O_2 undergoes a temperature increase and that leads to self-ignition. Thus, the ignition-delay-time difference between the pure-air case and the 12% O_2 diluted case equals $0.04 \mu\text{s}$. Figure 2(d) shows that self-ignition has also occurred for the case with 6% O_2 after $0.20 \mu\text{s}$ with a time delay difference, in comparison to the pure-air case, of about $0.14 \mu\text{s}$. In summary, it is observed that although the last case contained only 6% of O_2 , this amount did not delay significantly the self-ignition process in comparison with the undiluted case.

Figure 3 shows OH and H_2O mass fractions at $0.20 \mu\text{s}$. According to the chemical reaction mechanism by Burke et al. [13], O_2 and H_2 react and form the radical OH and H_2O in the chain-branching and

termination reactions, respectively. OH is produced first for the pure-air case, followed by the cases of 12% O₂ and 6% O₂, which are shown in Figure 3(a). It is also important to observe the peak positions where the OH is produced. The peak for pure air and the 6% O₂ case are located around the same positions at $x=10\ \mu\text{m}$, whereas the peak of OH for the case with 12% O₂ is located around $x=9.17\ \mu\text{m}$.

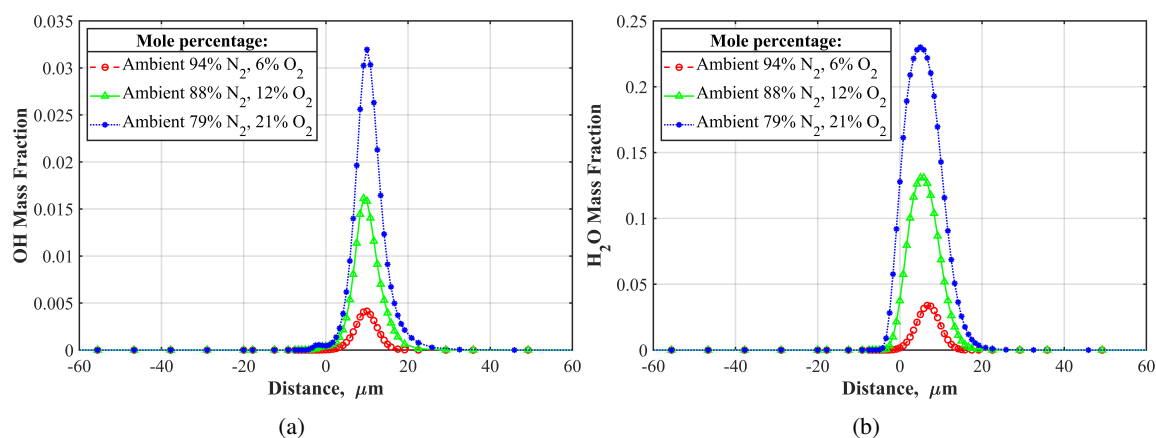


Figure 3: Species mass fraction profiles at $t=0.20\ \mu\text{s}$: (a) OH mass fraction, (b) H₂O mass fraction.

Figure 3(b) shows the production of water as a result of termination reactions, see [13]. Water is produced first in the pure-air case, followed by the 12% O₂ and 6% O₂ cases, respectively. Moreover, H₂O has a higher molar weight than OH; therefore, H₂O has a lower diffusion coefficient than OH [14]. As a result, H₂O diffuses less deep into the hot air region than OH. For example, the peak in mass fraction of H₂O occurs at $x=5\ \mu\text{m}$ for both the pure-air case and the 12% O₂ case, and at $x=6.67\ \mu\text{m}$ for the 6% O₂ case.

5 Conclusion

The aim of this work is to investigate the self-ignition process of pressurized hydrogen release into atmospheric air diluted with nitrogen. To achieve this goal, we used the open-source code Ember for conducting 1-D unsteady simulations of the mass and heat transfer as well as the chemical reactions at the reactive diffusion layer. The initial conditions mimic a pressurized jet release scenario and are derived by solving a shock-tube problem.

Analysis of the initial temperature profiles shows that nitrogen dilution on the air side has a negligible effect on the shock strength. It is thus demonstrated that the increase in ignition delay time is solely due to the chemical composition of the ambient. Nevertheless, the maximum difference in the ignition delay times, which occurs between the pure air case and the most diluted case with 6% O₂ is about 0.14 μs . Also, analysis of the H₂O and OH mass fractions reveals that the location where the peaks in mass fractions of H₂O and OH occur are not significantly affected by driven-gas dilution.

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