

Influence of Water Mist on Flame Acceleration, Transition to Detonation and Detonation Propagation in H₂-Air Mixtures

L. R. Boeck, A. Kink, D. Oezdin, J. Hasslberger and T. Sattelmayer
Lehrstuhl für Thermodynamik, Technische Universität München
Garching, Germany

1 Introduction

Explosion of H₂-air mixtures is an omnipresent risk in severe accident scenarios in nuclear power plants. Prediction of explosion impact on the containment of a nuclear reactor is complicated by uncertainty regarding initial conditions prior to ignition. The present study is part of a research project aiming at approaching real-world conditions during accidents in nuclear power plants. In the first part of the project, the influence of mixture inhomogeneity on flame acceleration [1], transition to detonation [2] and detonation propagation [3] has been studied. The second part, which is presented in this work, focuses on the influence of water mist on explosion processes in homogeneous H₂-air mixtures. Water loading ratios between 0.01 and 0.1 kg/m³ are relevant for severe accident scenarios in nuclear power plants.

Significant knowledge has been accumulated on gaseous explosions with water mist or water sprays, cp. review paper by Thomas [4]. The motivation of these investigations was mainly mitigation of explosion hazards in industrial applications by water sprays. Examined water loading ratios were often higher than relevant for nuclear reactor accident scenarios. In the majority of small and large scale studies available, reduction of explosion severity by sprays has been reported. Heating and evaporation of droplets causes a decrease in combustion temperature, lowering both the mixture burning velocity and the expansion ratio. Holborn et al. [5] and Battersby et al. [6] pursued an experimental approach for generating water mist very similar to the present study, employing ultrasonic atomizers. Battersby et al. determined a reduction in maximum overpressure of about 35 % with 0.09 kg/m³ water loading ratio in a 11.5 vol. % H₂-air mixture.

Our goal was to design an experiment with well-defined boundary conditions that allows for investigation of slow and fast deflagrations, transition to detonation and detonation propagation in H₂-air with water mist. Central requirements concerning water mist properties were: Defined droplet size distribution; Real-time measurement of water loading ratio; Homogeneous spatial droplet distribution.

2 Experimental Setup

2.1 Geometry and Measurement Techniques

Experiments were conducted in a classical explosion channel with a length of 4.2 m and a rectangular cross section (0.06 m height, 0.3 m width). The channel was equipped with flat plate obstacles with a

blockage ratio of 30 % at a spacing of 0.3 m. The first obstacle position is $x = 0.15$ m, the last $x = 4.05$ m. Piezoelectric pressure transducers (type Kistler 601A) were installed in the channel top plate (No. 1–5) and in the end plate (No. 6). Transducer positions are given in Tab. 1. This facility has been used in numerous studies before. Comprehensive information can be found in respective publications [1–3, 7].

Table 1: Distance of pressure transducers from point of ignition.

No.	1	2	3	4	5	6
x [m]	0.4	1.4	2.1	2.8	3.7	4.2

2.2 Generation of H₂–Air Mixture

For mixture preparation, the channel is first flushed with air. Second, the volume is partially evacuated to a predefined value p_{vac} , so that ambient pressure is reached after H₂ injection. Third, H₂ is injected through 126 evenly distributed ports in the top plate. Recirculation of H₂ and molecular diffusion leads to a quick homogenization of the mixture. From earlier experiments with concentration gradients, where a layer of H₂ was formed at the channel top and diffusion led to defined concentration gradients, it is known that a diffusion time t_d between injection and ignition of 60 s led to a homogeneous mixture [7]. Since we now inject H₂ perpendicularly without forming a layer, a shorter diffusion time is sufficient to reach homogeneity. In preliminary experiments it could be shown that diffusion times down to 5 s yield homogeneous mixtures. Overpressures during explosion in these mixtures are equal to overpressure after 60 s diffusion time within the measurement accuracy. We conducted all experiments presented in this work at a diffusion time of $t_d = 10$ s.

2.3 Water Mist Generation, Injection and Characterization

The explosion channel is equipped with a water mist injection system (Fig 1). Fourteen ultrasonic atomizers (1) are installed in a volume underneath the explosion volume (2), generating quiescent water mist. They are placed in cylinders (3) which are filled with water at a defined level. Water is provided through supply pipe (4) and removed by pipe (5) between the experiments. The water mist is transported into the explosion volume by an air flow generated by an external diaphragm pump (6), circulating air in a closed loop. The air flow is distributed between the atomizer units through a pipe system and is measured with a rotameter (7). Pressure losses in each branch were adjusted such that air flows through the units differ by less than ± 5 %. This was proven by constant temperature anemometry (CTA). Flowing into the cylinders at a flow rate of 17 l/min per atomizer unit, the air transports the water mist through inclined holes above each unit (8) into the explosion volume. Recirculating inside the volume, droplets distribute homogeneously. Air is recirculated towards the diaphragm pump through orifices in the bottom plate of the explosion volume (9). Water loading ratio is controlled by setting the time for water mist injection t_m .

Droplet size distribution is measured by laser scattering (MALVERN particle sizer). Fig. 2 (a) shows the distribution with a Sauter mean diameter (SMD) of 13 μm . Measurement of light extinction has been chosen to determine the water loading ratio. A diode laser (660 nm, 77 mW) operated at 40 mW is used as a light source. A beam splitter reflects part of the beam towards a reference photodiode, which is used for correcting temporal fluctuations of laser output power. The measurement beam is guided through windows into the explosion volume at $x = 2.17$ m. Behind the volume, the measurement photodiode detects transmitted light intensity. Photodiodes are connected to an sglux MULTIBOARD measurement amplifier. Diode and amplifier characteristics were calibrated by means of neutral density filters of

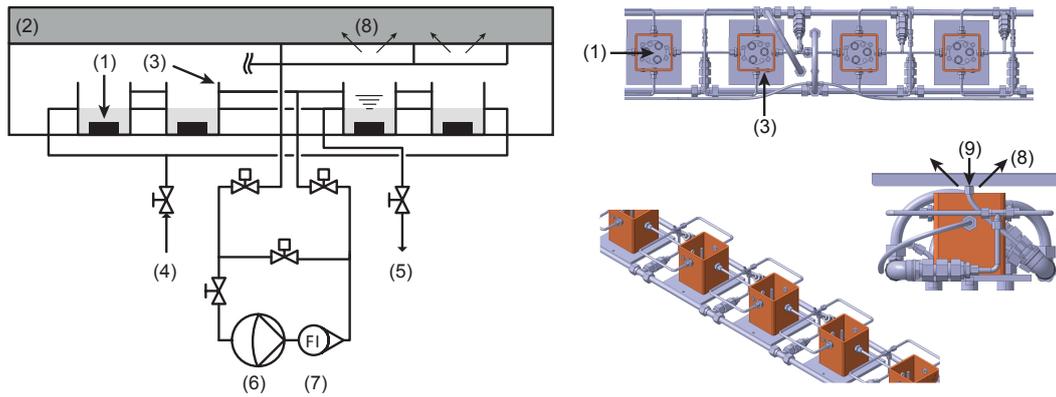


Figure 1: Water injection system. Not all fourteen atomizer units displayed.

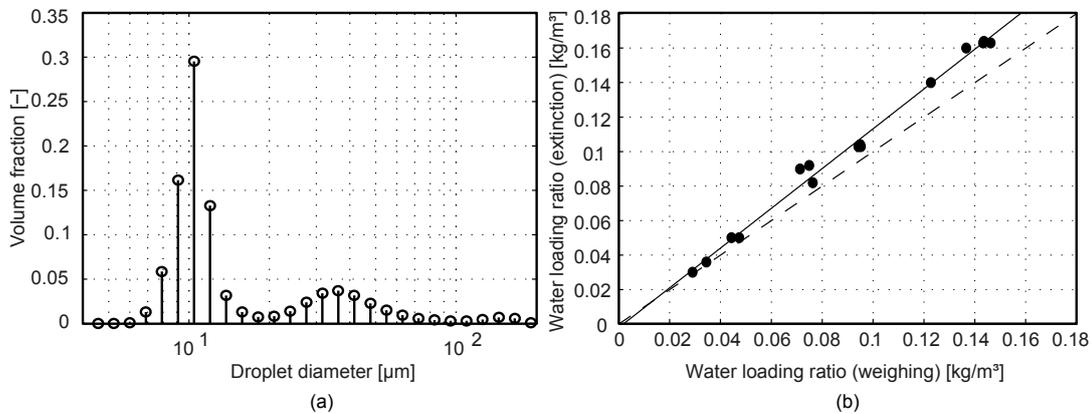


Figure 2: Droplet size distribution measured by laser scattering (a); Calibration of extinction measurement by weighing of samples (b).

known transmission at 660 nm. Employing the Beer-Lambert law, Eq. (1) [9], with the extinction coefficient σ_e according to Eq. (2), yields the particle number of concentration N as a function of intensity I measured behind and I_0 before light transmission through the water mist with the optical path length $L = 0.3$ m. Extinction efficiency Q_e is assumed constant, which is valid for particle sizes larger than $4 \mu\text{m}$ [9].

$$\frac{I}{I_0} = e^{-\sigma_e L} \quad (1)$$

$$\sigma_e = NQ_e A_p = \frac{NQ_e d^2 \pi}{4} \quad (2)$$

Since deviations from the Beer-Lambert law must be expected due to droplet sedimentation at the windows, and also due to multi-scattering effects at high water loading ratios, calibration of the extinction measurement technique was performed (Fig. 2 (b)). Samples with a volume of 380 ml were taken from the explosion volume and water mass weighed using a SORATORIUS MC 410 S scale. Initial conditions of the system (e.g. depositions on the windows) before water mist injection are taken into account through an automated calibration measurement before each experiment.

2.4 Experimental Procedure

The overall procedure for each experiment is as follows: Evacuation of the channel to p_{vac} ; Activation and calibration of extinction measurement; Channel flushing with water mist for time t_m ; Waiting time $t_w = 10$ s until water mist is quiescent; H₂ injection; H₂ diffusion time $t_d = 10$ s; Ignition - explosion (initial conditions for explosion: ambient pressure and temperature); Channel flushing with air for 180 s; Water refill for atomizers for 90 s; Water level equilibration for 150 s; Pipe system flushing with external air for 30 s. Each set of parameters (H₂ concentration X_{H_2} , water mist injection time t_m) was repeated three times.

3 Results

Three series of measurements were conducted: Reference experiments without water mist; Experiments with a water loading ratio of 0.06 kg/m³; Experiments at 0.11–0.12 kg/m³. In each of these groups, H₂ concentrations from 12.6 up to 19.2 vol. % were examined. This range covers phenomena from slow flames up to transition to detonation. Additionally, experiments in a near-stoichiometric mixture ($X_{H_2} = 30$ vol. %) were conducted to study detonation propagation.

3.1 Peak Overpressure

Figure 3 (a)–(c) shows peak overpressure at each pressure transducer depending on H₂ concentration in dry reference experiments (a), 0.06 kg/m³ (b) and 0.11–0.12 kg/m³ water loading ratio (c). From the comparison of (a) and (c), it is obvious that water mist reduces maximum overpressures and thus retards flame acceleration. Differences between (a) and (c) are well measurable, whereas differences between (a) and (b) lie within the measurement precision. At higher H₂ concentrations pressure transducers 4–6 showed tendencies of thermal shock in the measurements of (b), which may erroneously lower measured pressures at these transducers. Thus we focus on the comparison of (a) (“dry mixture”) and (c) (“wet mixture”).

Peak overpressures are lowered by water mist by up to 75 %, depending on pressure transducer position and H₂ concentration. Significant flame acceleration does not occur in dry and wet mixture at H₂ concentrations between 12.6 and 14.3 vol. % (overpressure remains fairly constant along the channel length). These experiments with slow flames are comparable to those presented by Battersby et al. [16], who found a reduction of peak overpressure of about 35 % between a dry mixture at $X_{H_2} = 11.5$ vol. % and a wet mixture with a 0.09 kg/m³ water loading ratio. Our measurements show a reduction of 23–36 % at pressure transducers 1–6 at 12.6 vol. % and 0.12 kg/m³. The added value of our study compared to [5, 6] is particularly the extension towards faster explosion regimes. Until pressure transducer 3, flames do not significantly accelerate even at elevated H₂ concentrations. It is insightful to study phenomena at 14.9 vol. % upwards at transducers 4–6. Relative comparison of overpressures of dry and wet mixture (Fig. 3 (d)) reveals that the effect of water mist on overpressure decreases with increasing H₂ concentration in the investigated range. The concentration of 14.9 vol. % is particularly interesting since water mist hinders transition from slow to fast flames here. Peak overpressure is 1.4 bar at the end plate in the wet experiment, while 5.5 bar is measured in the dry experiment. This equals a reduction of 75 %. We find that a water loading ratio of 0.11–0.12 kg/m³ causes a reduction of overpressure similar to a reduction of H₂ concentration by about 0.6 vol. % in the deflagration regime.

Phenomena at the end plate of the facility at pressure transducer 6 can be further evaluated. As we showed in [8], local explosions occur at the end plate as soon as deflagrations approach the end plate

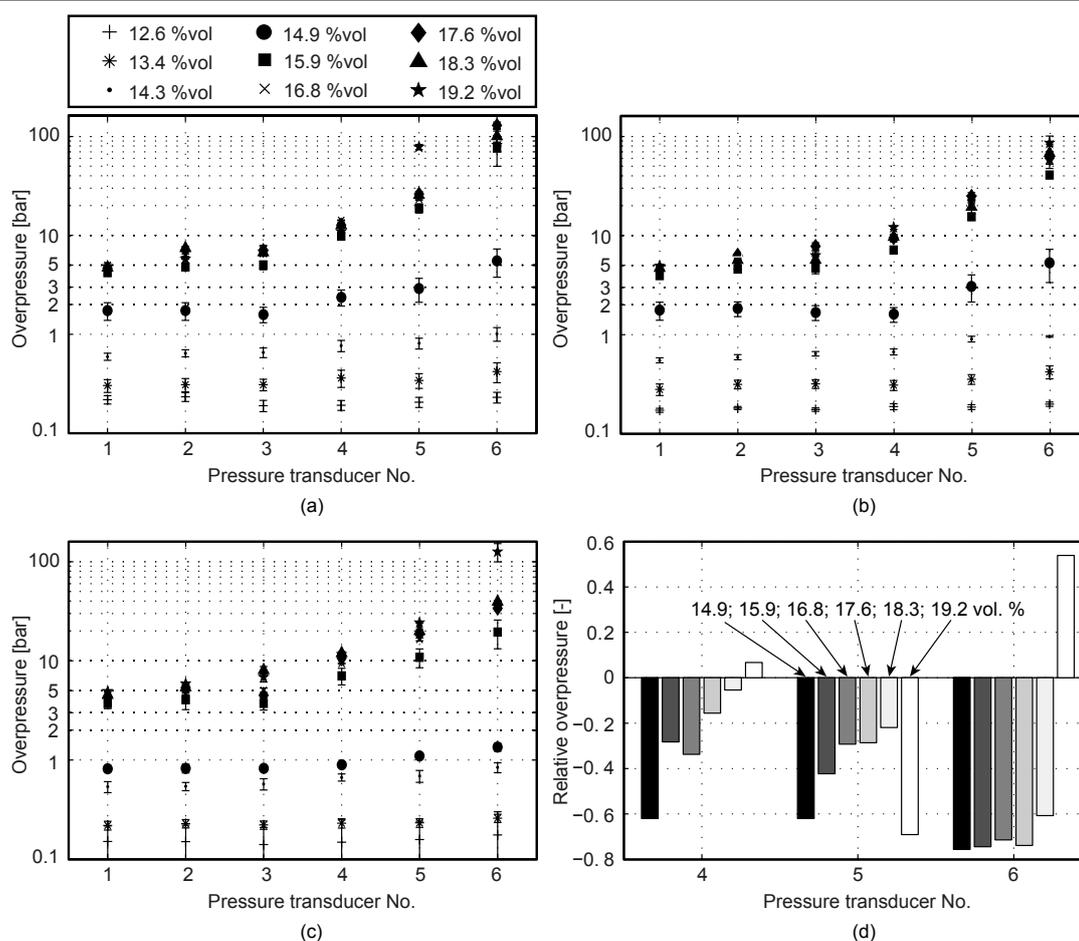


Figure 3: Peak overpressure without liquid water case 1 (a), water loading ratio 0.06 kg/m³ case 2 (b), 0.11–0.12 kg/m³ case 3 (c); relative difference in overpressure between wet (case 3) and dry (case 1) mixture at p₄–p₆ (d).

at a velocity close to the sound speed of the combustion products in the range of 800–1000 m/s. These explosions, initiating transition to detonation, cause overpressures of 100 bar and higher. Reflection of both slower deflagrations and detonations causes distinctly lower overpressure. In dry mixtures, such high peak pressures first occur between $X_{H_2} = 15.9$ and 16.8 vol. %. In the wet mixture, overpressure does not exceed 40 bar at H₂ concentrations of up to 18.3 vol. %. Only at 19.2 vol. % a high peak pressure of 125 bar is measured. In the dry mixture transition to detonation occurs close to transducer 5 at 19.2 vol. %, causing high overpressure. In the wet mixture, on the other hand, transition occurs at the end plate, yielding higher overpressure than effected by detonation reflection at the end plate in the dry mixture. This analysis clearly shows that water mist mitigates explosion hazards in the presented configuration by retarding transition from slow to fast flames and especially transition to detonation.

3.2 Detonation Velocity

Experiments in a near-stoichiometric mixture ($X_{H_2} = 30$ vol. %) were performed in order to investigate the influence of water mist on detonation propagation. Detonation velocity was determined from detonation arrival time at pressure transducers 4, 5 and 6. A water loading ratio of 0.12 kg/m³ was used.

In the dry reference mixture, a propagation velocity of 1984 m/s was measured, which almost equals the Chapman-Jouguet velocity for this mixture ($D_{CJ} = 1987$ m/s). Detonations in mixtures with water mist propagated at 1927 m/s, which equals a velocity deficit of about 3 % compared to the reference experiment. D_{CJ} of a dry mixture at 28 vol. % H₂ is 1922 m/s, so that the influence of water mist equals a reduction in X_{H_2} by 1–2 vol. %.

4 Concluding Remarks

The question has been posed by what extent water mist can influence explosion of H₂-air in severe accident scenarios. Experiments showed that water loading ratios around 0.11–0.12 kg/m³ mitigate explosion hazards through reduction of explosion overpressure. Measured reduction in overpressure equals the effect observed by reducing H₂ concentration by 0.6 vol. % in the deflagration regime and 1–2 % in the detonation regime.

The presented work is funded by the German Federal Ministry of Economic Affairs and Energy (BMWi) on the basis of a decision by the German Bundestag (project no. 1501338 and 1501425) which is gratefully acknowledged.

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