Explosion-Induced Ignition and Combustion of Acetylene Clouds

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1 Introduction

In the past, we have studied combustion effects in both confined [1],[2] and unconfined explosions [3]. And we have proposed gasdynamic models of turbulent combustion in TNT explosions [4]. Here we investigate the explosion-induced ignition and combustion of acetylene clouds in a retangular test chamber (Fig. 1). Chamber dimensions are: 101.5 mm x 101.5 mm x 386 mm. Gauges 1-5 were located on the centerline (y = 50.75 mm) at x = 43, 118, 193, 268 and 343 mm; gauges 6-10 were located near the side-wall (y = 20.75 mm) at the same axial locations. A spherical PETN charge (mass between 0.2 and 0.5 grams with a density of 1 g/cc) was inserted into the chamber from the left wall on a wand. Charge axial locations varied from x = 75 mm to 170 mm in different tests. The acetylene cloud was contained in a soap bubble film of various diameters (25, 40, 50 or 60 mm) typically located at x = 268 mm.



Figure 1. Photograph of the test chamber. In this test, a 0.5-g PETN-charge is place at x = 96.5 mm along the centerline (y = 50.75 mm) of the chamber. The air-filled soap bubble (d = 50 mm) is located at x = 268 mm.

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The charge was detonated by a high-voltage system described in [1]. This produced a blast wave that reflected from the walls, leading to complex Mach structures (Fig. 2: $t = 152 \,\mu s$). The Mach fronts crush the soap bubble ($t = 205 \,\mu s$) and deposit vorticity which causes turbulent mixing of the acetylene with air (Fig. 2: $259 \,\mu s < t < 312 \,\mu s$).



Figure 2. Schlieren photographs showing the evolution of a blast wave from a 0.3-g PETN charge, and its interaction with a 55-mm soap bubble filled with air.

2 Model

We model the system using the compressible Navier-Stokes equations for a reactive mixture [5], [6]. These equations express conservation of mass, momentum, total energy and species. If we assume unity Lewis number, so that species diffusion and thermal diffusion coefficients are the same, and ignore radiative effects, the system reduces to:

$$(\rho)_{t} + \nabla \cdot (\rho U) = 0$$

$$(\rho U)_{t} + \nabla \cdot (\rho UU) + \nabla p = \nabla \cdot \tau$$

$$(\rho E)_{t} + \nabla \cdot (\rho UE + pU) = \nabla \cdot \kappa \nabla T + \nabla \cdot h_{k} \rho D_{k} \nabla Y_{k} + \nabla \cdot \tau U$$

$$(\rho Y_{k})_{t} + \nabla \cdot (\rho UY_{k}) = \nabla \cdot (\rho D_{k} \nabla Y_{k}) + \dot{\omega}_{k}$$

where ρ , U, p, T and Y_k are density, velocity, pressure, temperature and mass-fraction of species k, respectively. Here E = e + UU/2 is the total energy and $e = \sum_k e_k(T)Y_k$ is the internal energy. The stress tensor $\tau = \mu (\nabla U + \nabla U^t) + \lambda I \nabla \cdot U$ where μ and λ are the viscosity coefficients and κ is the thermal conductivity. Lewis number of unity implies that the species mass diffusion $\rho D_k = \kappa / c_p$. For the simulations presented here we assume an ideal gas equation of state for the mixture: $p = \rho RT \sum_k Y_k / W_k$ where W_k is the molecular weight of species k. The formulation specifies the thermodynamic behavior of the system using a Chemkin interface and includes the capability ot model combustion as the ambient air mixes with the hydrocarbon cloud. Chemistry is modeled by a single-step reaction: $C_2H_2 + 2.5O_2 \rightarrow 2CO_2 + H_2O$:

$$\dot{\omega} = A e^{-E_a/RT} \left[C_2 H_2 \right]^{0.5} \left[O_2 \right]^{2.5}$$

PETN products are H_2O, CO_2, CO and N_2 .

The basic discretization uses a symmetric operator split formula in which we first advance the chemistry in each zone by $\Delta t/2$, then advance the Navier-Stokes equations without the reaction term by

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 Δt and finally advance the chemistry by $\Delta t/2$ again. The chemistry integration is performed using standard techniques for ordinary differential equations. The integration algorithm for the Navier-Stokes equations combines an explicit, second-order, unsplit Godunov method for the hyperbolic part of the operator with a second-order, explicit Runge-Kutta algorithm for the diffusive terms.

The integration algorithm is embedded in a hierarchial adaptive mesh refinement algorithm. In this approach, fine grids are formed by dividing coasrse cells by a refinement ration r, in each direction. Increasingly finer grids are recursively embedded in coasrse grids until the solution is adequately resolved with each level contained in the nest coasrser level. An error estimation procedure based on user-specified criteria where additional refinement is needed and grid generation procedures dynamically create or remove rectangular fine grid patches as resolution requirements change.

3 **Results**

The dynamics of the detonation products from a spherical 0.2-g PETN charge, and the ensueing ignition and combustion of a 50-mm acetylene bubble is depicted in Fig. 3. Cloud ignition occurs at $t = 0.55 \,\mu s$. It is this experiment that we have simulated with our compressible AMR code.

Figure 4 presents a three-dimensional volume rendering of the evolution of the temperature field of the acetylene cloud from the AMR simulation. It shows the flame dynamics in the turbulent combustion cloud.

Figure 5 compares the pressure histories at gauge 5 for three cases: (1) 50 mm diameter C_2H_2 bubble; (2) no bubble; and (3) AMR simulation. At early times (Fig. 5a), pressure histories in cases 1 and 2 are in close agreement, indicating that combustion has not influenced the flow (i.e., shock arrival times) at gauge 5 over that time domain. The AMR pressure record is in qualitative agreement with the data records. At later times (Fig. 5b), the pressure record from case 2 diverges from case 1; by 8 ms combustion has increased the pressure to ~3.3 bars (versus 1.5 bars for the no bubble case)—thereby illustrating the effect of energy release due to combustion in confined explosions. Beyond 8 ms, radiative losses begin to cool the fireball, thereby causing a gradual pressure decay. The pressure history from the AMR simulation is in qualitative agreement with measured pressure history for case 1 out to 8 ms, however the frequency content is somewhat lowere in the simulation.

4 Summary

The proposed AMR code model—based on the compressible Navier-Stokes equations for a reactive mixture—is able to capture the major features of ignition and evolution of turbulent combustion cloud in this problem. It would be interesting to study other experiments in this test series (different bubble diameters, different charge-bubble separations, etc.) to establish the limits of this modeling approach.

References

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Figure 3. Video photography of the dynamics of the detonation products from a spherical 0.2-g PETN charge at x = 130 mm, and the ignition/combustion of a 50-mm acetylene bubble located at x = 170 mm (Test #72); Framing rate = 9 kHz. $t_1 \sim 0.55 ms$.



Figure 4. Three-dimensional volume rendering of the temperature field of the acetylene cloud is used to visualize the flame dynamics in the turbulent combustion field from the AMR simulation (frame rate = 10 cylces). Temperature field of the PETN detonation products cloud has been removed in order to focus on acetylene combustion dynamics.



Figure 5. Pressure histories at gauge 5 for a 0.2-g spherical PETN charge detonated in the tunnel filled with air. Case 1: with an acetylene bubble (d = 50 mm), Case 2: no bubble; Case 3: 3D-AMR code simulation.