# Impact of Graphite dust on the explosion properties of $H_2/O_2/N_2$ mixtures

Jérémy SABARD<sup>\*,+</sup>, Yao-Chung HSU<sup>+,•</sup>, Mahmoud IDIR<sup>+</sup>, Nabiha CHAUMEIX<sup>+</sup>, Ahmed BENTAIB<sup>\*</sup>

 \* IRSN, PSN-RES/SAG/BPhAG, BP 17, 92262 Fontenay-Aux-Roses Cedex 2, France
<sup>+</sup> ICARE, CNRS Orléans, 1C Avenue de la recherche scientifique, 45071 Orléans Cedex 2
<sup>-</sup> Department of Aeronautics and Astronautics, National Cheng Kung University, Tainan, 70101, Taiwan, R.O.C.

## **1** Introduction

The international scientific program, for International Thermonuclear Experimental Reactor, ITER, is one of the first steps for mankind to create tremendous amounts of energy with the help of nuclear fusion. During the normal operation of ITER, a large amount of metallic dust and graphite particles are generated due to the interaction of the plasma with the vacuum vessel walls. In case of loss of coolant and/or vacuum accident scenario, water and/or air may enter the vacuum vessel (VV) of ITER facility. Subsequently, water will (i) vaporize leading to a pressure increase, (ii) react with graphite, beryllium and tungsten dust to generate H<sub>2</sub>. In the end, mixtures of  $H_2/O_2/N_2/dust$  can be obtained in the VV which can lead to flammable atmosphere which can be dangerous for the integrity of the ITER facility. In order to asses this risk, dedicated experiments have been performed to measure pressure loads of  $H_2/O_2/N_2$  mixtures and to investigate the impact of the dust concentration on these loads.  $H_2/O_2/inert$ gas mixtures have been the target of several studies for different initial temperatures: 300 K [1-5], 523 K [6] and different initial pressures from below the atmospheric one [3,4] up to 6 MPa [2,5,6]. But these studies concerned only the determination of the laminar flame speeds of these mixtures and none of them addressed conditions for which the ratio  $O_2/(O_2+N_2)$  was higher than 0.21. Only the study of Tang et al. [7] concerns the explosion parameters (explosion pressure, combustion duration, maximum rate of pressure rise) of hydrogen-air mixtures, diluted with nitrogen, over a wide range of equivalence ratios ( $\Phi$ =0.6-1.4) at elevated pressures (0.5 MPa) and temperatures (440 K). The dust may explode if an ignition source delivers enough energy to the mixture. Normally, the

energy level to ignite directly the two-phase dust-air mixture is higher than the homogeneous mixture. However, in two-phase mixtures, for example, a weak energy can ignite the gaseous phase which in turn will ignite the dust. In other words, the two-phase mixture is ignited by the flame of the hydrogenair flame rather than the weak source, like an electrical spark. So the importance of these kinds of studies reveals by degrees.  $H_2/O_2/N_2/graphite$  mixtures have been studied by Denkevits et al. [8,9]. They showed that the 4 µm diameter graphite particles were the most explosive ones. They measured the explosions parameters of  $H_2/O_2/N_2/graphite$  mixtures for hydrogen molar percent between 8 and 18 % mol in air at ambient temperature and 1 bar for graphite concentration until 250 g/cm<sup>3</sup>. They showed that for a hydrogen content equal or above 10 % mol, the dust can explode with the hydrogen and add extra overpressure that should be taken into account for the security of the ITER installation. The other interests in this issue are the possible negative effects of the dust on the explosion, that is, as

a heat sink, if less hydrogen or more dust are present. Since the dusts play a role of the inhibitant if the energy of the flame is not high enough to ignite them. The aim of the present work is to discriminate between the two possible regimes according to the initial conditions: temperature, pressure and composition.

# 2 Experimental setup and procedure

## 2.1 The spherical bomb

Two different spherical bombs, which differ only by their size (respectively 8.18 and 56 L), have been used during these experiments. The larger one (56 L) has been utilized for  $H_2/O_2/N_2$  mixtures experiments and the smallest one (8.18 L) for the two-phase ones. Each bomb is equipped with two opposite windows used to visualize the flame during its expansion. Each bomb is also equipped with a Kistler pressure sensor mounted flush with the inner surface of the vessel to measure the pressure variation during the combustion. This recording allows the determination of the maximum combustion pressure ( $P_{MAX}$ ) and the maximum pressure rise rate (dP/dt)<sub>MAX</sub> from which the deflagration index ( $K_G$  for the gas phase mixtures and  $K_{ST}$  for the gas-dust mixtures) is derived.  $P_{MAX}$  is also compared to the theoretical one which is calculated with the Equil Code of the Chemkin II library [10].

## 2.2 Ignition systems

The ignition source for this study is produced at the center of the spherical bombs either by (i) a spark initiated between 2 electrodes or (ii) the focusing of a pulsed laser beam (Figure 1).

When the spark ignition is used, for each run, the current and the high voltage of the electric discharge are measured via a current probe (Bergoz® CT-D1.0-B) and a high voltage probe (Tektronix® P6015A) respectively. The recording of these signals on a digitizing scope allows the estimation of the

energy deposited in the gaseous phase by the electric discharge: E = ||U \* I| dt. Two different sources

have been used. The first one delivers a weak energy, between 1 and 2 mJ, while the second one delivers energy around 20 mJ. In case of gaseous mixtures of  $H_2/O_2/N_2$ , the first ignition device was used since the energy deposited was more than needed to ignite the mixture. The second one was used when dust were added to the mixture.

In the case of laser ignition, the laser used is a prototype made by CILAS®. It consists of a Q-switched DPSS Nd-Yag laser working at 1064 nm with a pulse duration of 20 ns. It can deliver up to 90 mJ. The laser beam is  $TEM_{00}$  with a diameter of 3.2 mm and a M<sup>2</sup>=1.6. The laser energy delivered by pulse is adjustable via a variable attenuator. The laser latter consists of a half wave plate and a Glan-Taylor polarizer. In order to obtain sufficient laser energy densities at the focal point, before focusing, the beam diameter is expanded by a beam expander (Melles Griot<sup>®</sup>, HEB-4.0-10X) with a 10X magnification ratio. The energy delivered by the laser was measured for each test using a photodiode which receives only a small fraction of the incident beam before entering the spherical bomb. A careful calibration of this photodiode was performed using a laser Joule meter (Gentec®, QE12SP). A second photodiode was set to detect the occurrence of the laser induced breakdown in the center of the spherical bomb. A digital delay generator (BNC®, 575) is used to trigger the laser shot and the acquisition system of the camera. The maximum energy that could be reached is in the range of 60-70 mJ. Moreover, due to the electrical properties of graphite particles, the use of the laser beam to ignite the combustion proved to be easier than the spark between 2 electrodes. Indeed, it appeared that dust layer could cover the electrodes and their insulation parts inducing the formation of a short circuit. Hence, the maximum dust concentration for which the spark ignition is feasible was limited to 100  $g/m^3$ . In the case of laser ignition, concentrations as high as 330 g/m<sup>3</sup> have been reached.

## 2.3 Particle size meter

The particle size have been measured in real conditions injections (the injector is a cyclone system) with the help of a particle size meter HELOS from Sympatec®. The graphite particles have been bought from Alfa Aesar® with a purity of 99.9995%. The values obtained in these tests (SMD  $\approx$  17 - 18 µm) are higher than the one given by Alfa Aesar® (Manufacturer size: 2-15 µm). This difference

can be explained by the measurement protocol and by the particles agglomeration that could happen during the injection process.

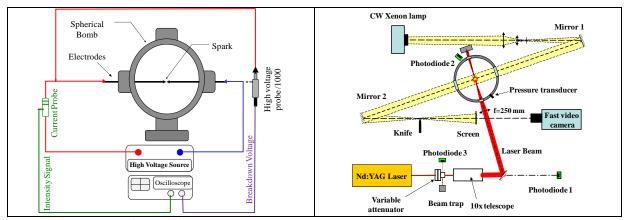


Figure 1: Scheme of the different ignition systems. On the left: spark ignition; On the right: laser beam focalization

### 2.4 Injection system and validation of the dust concentration by laser extinction

For the two-phase mixtures experiments, the filling of the spherical bomb was done with the help of mass flow meter for the gas phase. A cyclone (25mm i.d. and 100mm in length) is used for the injection of the dusts. The dust concentration is calculated directly from the gravimetric measurements of the cyclone before and after each test. However due to sticky properties of graphite and to the velocity of the flow during the filling procedure, the graphite mass that is really in suspension can be different from the mass released by the cyclone. Part of this mass can be lost to the walls. In order to limit these dust losses, the filling procedure has been carefully optimized. Before the starting of the injection, all the system (spherical bomb, pipeline and cyclone) is vacuumed. Two stages of injection are used in order to obtain the best dispersion of the dusts. A rough evaluation of the dust concentration in the bomb is made through extinction measurement using a 3.3  $\mu$ m HeNe laser and a fast HgCdTe detector. We could measure a linear dependence of the extinction coefficient for dust concentrations, determined through initial graphite mass derived from the gravimetric measurements of the cyclone, lower than 22.5 g/m<sup>3</sup>. However, the maximum concentration graphite used in this study is 330 g/m<sup>3</sup>.

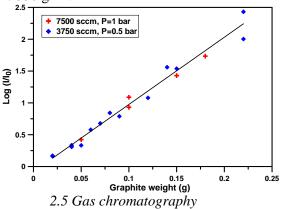


Figure 2: The ratio of transmitted intensity to the incident intesity in a logarithm versus the the dust weight

In order to characterize the burnt gases composition for the two-phase mixtures experiments, after each experiment, a sample was taken using a 1 L glass bulb and analyzed off-line with a gas chromatographer (HP 6890). The chromatographer is equipped with two columns. The first one is a

molecular sieve with a porosity of 5 Å which allows the separation of  $H_2$ , CO, CH<sub>4</sub>, O<sub>2</sub> and N<sub>2</sub> and the second one is a HP-Plot Q with a mixture of divinylbenzene and styrene with porosity equals to 40Å. This column permits the separation of the CO<sub>2</sub>. A TCD detector is added to the gas chromatographer for the analysis. A system of injection is installed near the GC which allows us to inject the samples and the standard ones at the desired pressure.

2.6 *Experimental conditions* 

For the  $H_2/O_2/N_2$  study, the  $H_2$  content has been ranged from 10 to 60 % mol, for 2 initial temperatures (303 and 343 K) and 2 initial pressures (50 and 100 kPa). The molar ratio  $N_2/O_2$  was varied from 0.66 up to 9. In the following,  $H_2$  content reported was calculated by considering its molar fractions:  $\% H_2 = x_{H2}/[x_{H2}+x_{O2}+x_{N2}])$ . For the two-phase  $H_2/O_2/N_2$ /graphite mixtures, the  $H_2$  content has been varied between 10 and 30 % mol, for two initial pressures (50 and 100 kPa) at 300 K. Two molar ratios  $N_2/O_2$  have been studied: 2.33 and 3.76 for dust concentrations from 0 to above 300 g/m<sup>3</sup>.

## **3** Results

## 3.1 Gaseous $H_2/O_2/N_2$ mixtures

As a first step, the combustion properties of gaseous  $H_2/O_2/N_2$  mixtures were measured for different conditions of initial temperature (303 and 343 K), initial pressure (0.5 and 1 bar), hydrogen molar fraction (0.1-0.6) and of dilution ( $N_2/O_2=2.33$ ; 3.76; 9). Maximum pressure was measured and compared to the theoretical value for an adiabatic isochoric complete combustion ( $P_{AICC}$ ).

The evolution of the experimental maximum pressure versus the molar fraction of  $H_2$  follows a bell shape curve (Figure 3). A good agreement between the measurements and the calculation is obtained over all the studied range. The difference between  $P_{MAX}$  and  $P_{AICC}$  is between 1.7 and 9 %. The maximum derivation is observed for the more diluted mixtures. In this case, the combustion time is very large compared to the last diluted one and hence the heat losses are more preeminent. For both initial temperatures,  $P_{MAX}$  reaches its highest value at a hydrogen molar fraction that depends on the  $N_2/O_2$  ratio. For  $N_2/O_2$  of 9, the maximum is at  $XH_2$ =0.2 and it is shifted to 0.3 and 0.4 when the  $N_2/O_2$  decreased to 3.76 and 2.33 respectively.

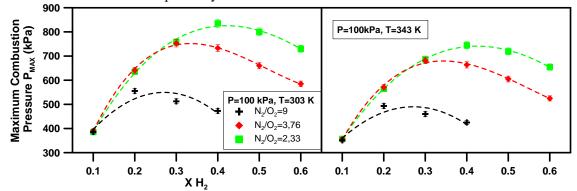


Figure 3: Maximum combustion pressure ( $P_{MAX}$ ) for  $H_2/O_2/N_2$  mixtures in function of the molar fraction in  $H_2$  at 100 kPa and for two initial temperatures: 303 and 343 K

#### 3.2Dust behavior in two-phase mixtures

As graphite particles are added to the mixture, the combustion of this two-phase media will depend strongly on the hydrogen molar fraction since the ignition energy deposited by either the spark generated between 2 electrodes or by the laser is below the critical ignition energy of graphite/air mixtures. For these experiments gaseous samples of the burnt gases were taken after each test and analyzed using a gas chromatographer (Table 1). Since the gaseous fuel is hydrogen and carbon is present only as graphite, the presence of CO and/or  $CO_2$  in the burnt gases is a good indicator that the particles have burnt due to the flame of hydrogen.

SABARD J.				Explosions properties of H <sub>2</sub> /O <sub>2</sub> /N <sub>2</sub> /Graphite mixtures					
H <sub>2</sub> fraction	0.1		0.2		0.3				
N <sub>2</sub> /O <sub>2</sub>	2.33	3.76	2.33	3.76	2.33	3.76			
[Graphite] (g/m <sup>3</sup> )	98.75	98.75	98.75	83.75	77.5	25	48.75	88.75	162.5
Φ	0.934	1.345	1.265	1.634	1.452	1.356	1.679	2.225	3.231
GC results for burnt gases									
H <sub>2</sub>	0	0	0	0	4.85	7.04	7.39	8.31	8.37
CO	0	0	0	0	4.3	1.2	1.43	1.88	1.89
CO <sub>2</sub>	0	0	7.85	5.17	8.56	1.45	1.72	1.92	1.92
O <sub>2</sub>	24.87	16.72	10.51	5.97	0	1.28	1.36	1.46	1.53

Explosions properties of H<sub>2</sub>/O<sub>2</sub>/N<sub>2</sub>/Graphite mixtures

Table 1: Analysis of the burnt gases by GC for two-phase mixtures.

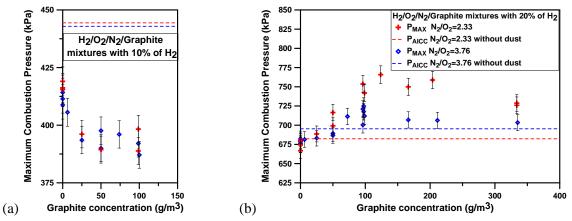


Figure 4: P<sub>MAX</sub> and P<sub>AICC</sub> for H<sub>2</sub>/O<sub>2</sub>/N<sub>2</sub>/Graphite mixtures with (a) 10 and (b) 20% mol in hydrogen in function of the graphite concentration at 300 K and 1 bar

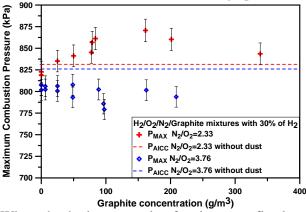


Figure 5: P<sub>MAX</sub> and P<sub>AICC</sub> for H<sub>2</sub>/O<sub>2</sub>/N<sub>2</sub>/Graphite mixtures with 30% mol in hydrogen in function of the graphite concentration at 300 K and 1 bar

When the hydrogen molar fraction was fixed at 0.1, PMAX was lower than both PMAX,no dust and  $P_{AICC.no.dust}$ , and decreased as the initial graphite content increased in the spherical bomb (Figure 4a). Moreover the analysis of the burnt gases did not show any H<sub>2</sub>, CO or CO<sub>2</sub> in the sample (Table 1). Hence, when the hydrogen molar fraction is equal to 0.1, the combustion of the gaseous phase does not ignite the graphite particles, but these acts as a heat sink and therefore the maximum pressure is lower. This behavior is observed for both  $N_2/O_2$  ratios of 3.76 and 2.33.

As the molar fraction of hydrogen is increased to 0.2, the presence of graphite particles induces an increase of P<sub>MAX</sub> and the obtained values are higher than the corresponding P<sub>AICC,no dust</sub> (Figure 4b). For example, at XH<sub>2</sub>=0.2 and N<sub>2</sub>/O<sub>2</sub>=2.33, the mixture with a graphite concentration equals to 124 g/m<sup>3</sup> gives a  $P_{MAX}$  equals to 766 kPa which is 90 kPa higher than  $P_{AICC,no}$  dust. Moreover, the gas chromatography analyses show that the burnt gases are constituted of CO and CO<sub>2</sub>. No H<sub>2</sub> could be

detected (Table 1). Then for 20 % mol H<sub>2</sub> in the mixture, the initial hydrogen combusted totally and the graphite particles have also burnt. This behavior is observed for both  $N_2/O_2$  ratios of 3.76 and 2.33. As the hydrogen molar fraction is up to 0.3, the behavior of the graphite particles is not the same for the different  $N_2/O_2$  ratios (Figure 5). For the ratio  $N_2/O_2=2.33$ , it is the same than the one observed at 20 % mol  $H_2$ , which leads us to conclude that the dust burns. It is corroborated by the results of the analysis of the burnt gases. The results show that CO<sub>2</sub>, CO and H<sub>2</sub> are present in the burnt gases (Table 1). The presence of  $H_2$  can be explained by the fact that when more dust is added, the mixtures begin to become rich in combustible and there is a competition between  $H_2$  and graphite for burning. For the mixtures at N<sub>2</sub>/O<sub>2</sub>=3.76, the P<sub>MAX</sub> behavior is different. Indeed, for the entire studied domain, it remains almost constant. The first supposition is that the mixture is too rich and only hydrogen burns because it is supposedly easier to be ignited and the mixture is so fast that the particles do not have enough time to play as heat sinks. However, CO, CO<sub>2</sub>, H<sub>2</sub> and O<sub>2</sub> are detected in the burnt gases, which indicate the incompleteness of the combustion (Table 1). In the early stage of the combustion, only hydrogen burns but the combustion is so powerful that the graphite begins to burn rapidly and consumes the remaining oxygen in the mixture. A first visualization, not detailed here, of these experiments supports the ignition in two steps. For example, in the mixture with [Graphite]=162.5  $g/m^3$ , almost 2 % mol of CO and CO<sub>2</sub> were found in the burnt gases and also 8.3 % mol of H<sub>2</sub> (Table 1). In this particular case, almost one-third of the hydrogen is remaining. These two phenomena, the burnt dust and unburnt hydrogen, lead to a pressure profile of  $P_{MAX}$  which remains almost flat.

# 4 Conclusion

In this work, new experimental data concerning the combustion properties were acquired in a spherical vessel of  $H_2/O_2/N_2$  and  $H_2/O_2/N_2$ /Graphite mixtures which are related to the explosion risk assessment in the ITER project. The impact of the  $N_2/O_2$  ratio in the mixture was observed as well as the impact of the presence of dust. For mixtures with 10% mol of hydrogen, the  $P_{MAX}$  are always below the  $P_{AICC}$  of the mixture without dust and composition of the burnt gases shows that the dusts did not burn in the mixture. However, in the 20 and 30 % mol  $H_2$  cases, the dusts burn with the evidence of the  $P_{MAX}$  and composition of the burnt gases, at the exception of 30 % mol  $H_2$  in air. In this particular case, both the  $H_2$  and the graphite have been ignited and their combustion was incomplete since the overall equivalence ratio is higher than one. However, around 1 % of  $O_2$  is found in the burnt gases.

# Acknowledgment

The authors thank the Région Centre and the IRSN for their financial support of this work.

# References

- 1. Ratna Kishore V. et al. (2009). Adiabatic burning velocity of  $H_2$ -O<sub>2</sub> mixtures diluted with CO<sub>2</sub>/N<sub>2</sub>/Ar. Int. J. Hydrogen Energy. 34: 8378.
- 2. Tse S.D. et al. (2000). Morphology and burning rates of expanding spherical flames in  $H_2/O_2$ /inert mixtures up to 60 atmosphere. Proc. Combust. Institute 28: 1793.
- 3. Qiao L. et al. (2005). Suppression effects of diluents on laminar premixed hydrogen/oxygen/nitrogen flames. Combust. Flame 143: 79.
- 4. Qiao L. et al. (2007). A study of the effects of diluents on near-limit H2-air flames in microgravity at normal and reduced pressure. Combust. Flame. 151: 196.
- 5. Aung K.T. et al. (1998). Effects of pressure and nitrogen dilution on flame/stretch interactions of laminar premixed H<sub>2</sub>/O<sub>2</sub>/N<sub>2</sub> flames. Combust. Flame. 112: 1.
- 6. Shebeko Y.N. et al. (1995). Burning velocities and flammability limits of gaseous mixtures at elevated temperatures and pressures. Combust. Flame 102: 427.
- 7. Tang C. et al. (2009). Int. J. Hydrogen Energy 34: 554.
- 8. Denkevits A. (2007). Explosibility of H<sub>2</sub>-graphite dust mixtures. J. of Loss Prevention 20: 698.
- 9. Denkevits A. et al. (2005). Dust explosion hazard in ITER. Fusion Engi. Design 75-79: 1135.
- 10. Kee R.J. et al. (1993). Report no. SAND89-8009B, Sandia International Laboratories.
  - 24<sup>th</sup> ICDERS July 28 August 2, 2013 Taiwan